ELEC4410

Control System Design

Lecture 7: Introduction to MIMO Systems

School of Electrical Engineering and Computer Science The University of Newcastle



MIMO Systems



- MIMO Systems
- Transfer Matrices, Poles and Zeros

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- Stability



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- Interaction, Decoupling and Diagonal Dominance



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References: Control System Design, Goodwin, Graebe & Salgado. Multivariable Feedback Control: Analysis and Design, Skogestad & Postlethwaite.

MIMO Systems

Up to now we have assumed that a control problem can be reduced to controlling a single "control variable" with a single "manipulated variable". The two are assumed to be related via some simple (linear) dynamics, for example, a transfer function

 $Y(s)=G(s)U(s), \quad \text{where } Y\!,G,U:\mathbb{C}\mapsto\mathbb{C}.$



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- However, in most cases, a system has more than one manipulated variable and more than one control input, and the interactions between these are such that the model cannot be further reduced.
- A system in which the input and the output are vectors, rather than scalars, is a system with Multiple Inputs and Multiple Outputs (a MIMO system), sometimes also called a multivariable system.

Example: Control of an Aircraft

Wilbur Wright said in 1901:

Men know how to construct airplanes. Men also know how to build engines. Inability to **balance** and **steer** still confronts students on the flying problem. When this one feature has been worked out, the age of flying will have arrived, for all other difficulties are of minor importance.



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The Wright Brothers solved the control problem and flew the Kitty Hawk on december 17, 1903.



Example: Control of an Aircraft

The Wright Brothers had to solve a MIMO control problem!





Example: Copper Heap Bioleaching

Heap bioleaching is a process used to extract copper and other metals from large amounts of heaped ore with low grade content, based on the action of chemolithotrophic bacteria.





Example: Copper Heap Bioleaching

Heap bioleaching is a complex MIMO process with many interacting variables, among many others:

- Raffinate concentration
- Temperature and pH gradient
- Pump Raffinate \rightarrow Raffinate drip lines Λ 1 Ore leaching Blower Air Heap of crushed copper sulfide ore $PLS \rightarrow$ Forced aireation lines Impervious liner 2 Metallic Cu extraction Raffinate pond PLS pond \leftarrow \leftarrow Copper extraction plant Fe oxidation 3 > Copper for industrial use
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Bacteria population

Oxygen flow

Transfer Matrices

When a MIMO system can be represented by a LTI model, we can use an external representation that extends the idea of a transfer function: a transfer matrix function

$$\begin{bmatrix} Y_1(s) \\ Y_2(s) \\ \vdots \\ Y_q(s) \end{bmatrix} = \begin{bmatrix} G_{11}(s) & G_{12}(s) & \cdots & G_{1p} \\ G_{21}(s) & G_{22}(s) & \cdots & G_{2p} \\ \vdots & \vdots & \ddots & \vdots \\ G_{q1}(s) & G_{q2}(s) & \cdots & G_{qp} \end{bmatrix} \begin{bmatrix} U_1(s) \\ U_2(s) \\ \vdots \\ U_p(s) \end{bmatrix}$$



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• We can still write

$$\mathbf{Y}(\mathbf{s}) = \mathbf{G}(\mathbf{s})\mathbf{U}(\mathbf{s}),$$

but now $Y \in \mathbb{C}^q$, $U \in \mathbb{C}^p$, and $G \in \mathbb{C}^{q \times p}$. Besides **gain** and **phase** in G(s), for MIMO systems also **directions** play a fundamental role.

The Four Tank Apparatus is a laboratory system useful to study MIMO systems.

It is a system with two inputs (the flows u_1 and u_2 provided by the pumps) and two outputs (the levels y_1 and y_2 of the two lower tanks).





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At a suitable operating point, the system can be described by the transfer matrix

$$G(s) = \begin{bmatrix} \frac{3.7\gamma_1}{62s+1} & \frac{3.7(1-\gamma_2)}{(23s+1)(62s+1)} \\ \frac{4.7(1-\gamma_1)}{(30s+1)(90s+1)} & \frac{4.7\gamma_2}{90s+1} \end{bmatrix}$$



The poles of a multivariable system are the poles of the elements of the transfer matrix.

Example. Take the transfer matrix of the four tank apparatus,

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Then the poles of G(s) lie at

$$p_1=-1/62, \quad p_2=-1/23, \quad p_3=-1/30, \quad p_4=-1/90.$$



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Then the poles of $\mathbf{G}(\mathbf{s})$ lie at

$$p_1 = -1/62, \quad p_2 = -1/23, \quad p_3 = -1/30, \quad p_4 = -1/90.$$

It is less straightforward to tell the multiplicity of the poles. One way to do it, if the system is square, is via the computation of the **determinant** of G(s).

The multiplicity of the poles of a MIMO system, if it has the same number of inputs and outputs, can be found from the determinant of the transfer matrix.

Example. Consider again the four tank apparatus. Then

$$\begin{aligned} \det G(s) &= \det \begin{bmatrix} \frac{3.7\gamma_1}{62s+1} & \frac{3.7(1-\gamma_2)}{(23s+1)(62s+1)} \\ \frac{4.7(1-\gamma_1)}{(30s+1)(90s+1)} & \frac{4.7\gamma_2}{90s+1} \end{bmatrix} \\ &= \frac{3.7}{(62s+1)} \frac{4.7}{(90s+1)} \left(\gamma_1 \gamma_2 - \frac{(1-\gamma_1)(1-\gamma_2)}{(30s+1)(23s+1)} \right) \\ &= \frac{3.7 \times 4.7}{(62s+1)(90s+1)} \left(\frac{\gamma_1 \gamma_2 (30s+1)(23s+1) - (1-\gamma_2)(1-\gamma_1)}{(30s+1)(23s+1)} \right) \end{aligned}$$

We see that all the poles of G(s) have multiplicity 1. \Box



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We see that all the poles of G(s) have **multiplicity 1**.

If the system is not square, then the multiplicity of the poles of G(s) can be found from a minimal state space representation.

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Example. Consider the transfer matrix

$$G(s) = \begin{bmatrix} \frac{4}{(s+1)(s+2)} & \frac{-1}{(s+1)} \\ \frac{2}{(s+1)} & \frac{-1}{2(s+1)(s+2)} \end{bmatrix}$$

We can see that it has poles at $p_1 = -1$ and $p_2 = -2$. To find their multiplicity we compute the determinant of G(s),

$$\det G(s) = \frac{-4}{2(s+1)^2(s+2)^2} + \frac{2}{(s+1)^2}$$
$$= \frac{2}{(s+1)^2} \left(1 - \frac{1}{(s+2)^2}\right) = \frac{2\left[(s+2)^2 - 1\right]}{(s+1)^2(s+2)^2}$$
$$= \frac{2(s+3)(s+1)}{(s+1)^2(s+2)^2} = .$$



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Thus there is one pole at s = -1 and two poles at s = -2.



Zeros of a MIMO system

There are many definitions of zeros for MIMO systems. The most useful one that of a **transmission zero**, which can be (loosely) defined as a pole of the inverse plant (for square plants). **Example.** Consider again the transfer matrix of the previous

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Because $det[G(s)^{-1}] = det[G(s)]^{-1}$, we can obtain the zeros of G(s) as the zeros of det[G(s)]. From the previous Example

det G(s) =
$$\frac{2(s+3)}{(s+1)(s+2)^2}$$
.

Thus G(s) has a zero at s = -3. Again, more sophisticated methods should be used if the transfer matrix is not square.

Stability of MIMO Systems

Stability for MIMO systems is as for SISO systems.

A continuous-time multivariable system is stable if and only if all its poles lie in the **left** half plane.



(a) Continuous-time

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- A continuous-time multivariable system is stable if and only if all its poles lie in the **left** half plane.
- A discrete-time multivariable system is stable if and only if all its poles lie **inside** the unit circle.



Minimum Phase MIMO Systems

As for a SISO system, a MIMO system is said to be minimum phase if it has no zeros outside the stability region. Otherwise, it is called nonminimum phase.

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Example. Consider again the four tank apparatus system. It is not difficult to show that the system has two multivariable zeros that satisfy det[G(s)] = 0 at the roots of

$$(23s+1)(30s+1) - \eta = 0$$
, where $\eta = \frac{(1-\gamma_1)(1-\gamma_2)}{\gamma_1\gamma_2}$.

The system is nonminimum phase if $\eta > 1 \Leftrightarrow (\gamma_1 + \gamma_2) < 1$.

Interaction and Decoupling

One of the most challenging aspects of the control of MIMO systems is the interaction between different inputs and outputs.

In general, each input will have an effect on every output of the system (outputs are coupled). Take for example a 2×2 system

$$\begin{bmatrix} Y_1(s) \\ Y_2(s) \end{bmatrix} = \begin{bmatrix} G_{11}(s) & G_{12}(s) \\ G_{21}(s) & G_{22}(s) \end{bmatrix} \begin{bmatrix} u_1(s) \\ u_2(s) \end{bmatrix}$$
$$= \begin{bmatrix} G_{11}(s)U_1(s) + G_{12}(s)U_2(s) \\ G_{12}(s)U_1(s) + G_{22}(s)U_2(s) \end{bmatrix}$$


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When the MIMO system is such that each input only affects one particular output, different from the outputs affected by other inputs, the system is decoupled or noninteracting.

Because of coupling, in MIMO systems signals can interact in unexpected ways.



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Both outputs will be affected!

If G(s) is a diagonal matrix, the MIMO system is totally decoupled. The MIMO control design problem then reduces to several SISO control design problems.

For example, we could implement IMC for each loop separately.

$$K_{i}(s) = \frac{Q_{i}(s)}{1 - Q_{i}(s)G_{ii}(s)}$$



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- Loosely, a diagonally dominant plant has a transfer matrix in which the transfer functions on the diagonal are greater in magnitude than the off-diagonal elements.











A plant can sometimes be **made** to be diagonally dominant, at least at some critical frequencies.

One possibility is to achieve decoupling at DC by making G(0) diagonal using a static pre-compensator at the input of the plant P = G⁻¹(0), so that PG(0) = I.





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For the four tank example, the pre-compensator is

$$P = \begin{bmatrix} 3.7\gamma & 3.7(1-\gamma) \\ 4.7(1-\gamma) & 4.7\gamma \end{bmatrix}^{-1}$$
$$= \frac{1}{3.7 \times 4.7(2\gamma-1)} \begin{bmatrix} 4.7\gamma & 3.7(\gamma-1) \\ 4.7(\gamma-1) & 3.7\gamma \end{bmatrix}$$



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The figure below shows the Bode magnitudes of the four tank apparatus, with and without precompensation for DC decoupling, for $\gamma = 0.75$.





If a plant transfer matrix is diagonally dominant, it may be possible to design a good controller by considering each input-output pair as a separate loop. This approach is sometimes called **decentralised control**.

An important issue in decentralised control design is the appropriate selection of input-output pairs (Note that they will not in general be arranged so that G(s) is diagonal).

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- An important issue in decentralised control design is the appropriate selection of input-output pairs (Note that they will not in general be arranged so that G(s) is diagonal).
- One way of choosing the pairing is via the relative gain array (RGA) Λ, given by

$$\Lambda = \mathbf{G}(\mathbf{0}) \cdot \mathbf{G}^{-1}(\mathbf{0})^{\mathsf{T}}$$

where .* denotes element-wise multiplication.



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where .* denotes element-wise multiplication.

Each row and column in the RGA always sums to 1, and the values are independent of units (e.g., A or mA, m or mm).

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Example. For the four tank apparatus

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SO

$$\Lambda = \begin{bmatrix} \lambda & 1 - \lambda \\ 1 - \lambda & \lambda \end{bmatrix}, \quad \text{with } \lambda = \frac{\gamma_1 \gamma_2}{\gamma_1 + \gamma_2 - 1}$$



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If $\gamma_1 = \gamma_2 = \gamma$, and $\gamma = 1$, the RGA rule suggests the pairing (u_1, y_1) and (u_2, y_2) . On the other hand, if $\gamma = 0$, the pairing suggested is the opposite, (u_1, y_2) , (u_2, y_1) .



MIMO Sensitivity Functions

Consider a closed-loop system



The difference with SISO systems is that G(s) and K(s) are now **transfer matrices**, so we must be more careful with their algebraic manipulation (matrix products do not commute).



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As for SISO systems, we define

- $S = (I + GK)^{-1}$: The (nominal) Sensitivity
- $T = (I + GK)^{-1}GK$: The (nominal) Complementary Sensitivity

Sensitivities are very useful to specify and analyse performance and robustness of feedback control systems.

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- However, it is certainly difficult to specify desired performance for n × n scalar transfer functions, if say we have a n-input n-output plant.
- We often obtain more useful results if we consider the principal gains rather than the gains of each element in the transfer function matrix.
- The principal gains are the singular values of the complex transfer function matrix.

$$\sigma_{i}(j\omega) = \sqrt{\text{eig}[G(j\omega)G^{H}(j\omega)]}$$

where $(.)^{H}$ denotes the conjugate transpose.

The figure shows the principal gains for the four tank example for $\gamma = 0.95$ and $\gamma = 0.5$.



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If we have a result for a SISO (single-input single-output) system requiring an upper bound on a certain gain, then it is likely to generalise to a MIMO (multivariable) system as requiring an upper bound on the corresponding **maximum principal gain**.

 $\sigma_{\text{max}}(j\omega) = \max_{i} \sigma_{i}(j\omega)$

For the SISO case good tracking in some bandwidth $0 \le \omega \le B$ requires $T \approx 1$. This in turn requires $S \approx 0$ in the corresponding bandwidth.

For the MIMO case this becomes the requirement $\sigma_{max}(S)\approx 0$ within that range of frequencies. This is equivalent to the requirement that

$$T \approx I$$
, for $\omega \in [0, B]$

In MATLAB the principal gains can be computed with the



The generalisation of IMC design methodology for **square** MIMO systems is straightforward. The parameterisation of all controllers that yield a stable closed-loop system for a stable plant with nominal model $G_0(s)$ is given by

 $K(s) = [I - Q(s)G_0(s)]^{-1}Q(s) = Q(s)[I - G_0(s)Q(s)]^{-1},$

where Q(s) is any stable proper transfer matrix.



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where Q(s) is any stable proper transfer matrix.

Example. Consider again the 2-input, 2-output plant represented by

$$G(s) = \begin{bmatrix} \frac{4}{(s+1)(s+2)} & \frac{-1}{(s+1)} \\ \frac{2}{(s+1)} & \frac{-1}{2(s+1)(s+2)} \end{bmatrix}$$



Example (continuation).

As seen before, this plant is stable and minimum phase, with poles at s = -2, -2, -1 and a zero at s = -3. Because the only zero is in the left half plane, the plant is relatively easy to control.

To implement an IMC design, note that

$$G^{-1}(s) = \frac{(s+2)^2}{2(s+3)} \begin{bmatrix} \frac{-1}{s+2} & 1\\ -2 & \frac{4}{s+2} \end{bmatrix},$$



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So a sensible choice for Q(s) might be

$$Q(s) = \frac{(s+2)^2}{2(s+3)(\lambda s+1)} \begin{bmatrix} \frac{-1}{s+2} & 1\\ -2 & \frac{4}{s+2} \end{bmatrix}, \quad \text{for some } \lambda > 0.$$



Example (continuation). We implement in Simulink this IMC design for $\lambda = 1$, including step references and input disturbances.





Example (continuation). The plots show the response of the closed-loop system to input step references and disturbances.




MIMO Control Design

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However, in general the choice of a suitable matrix $\mathbf{Q}(\mathbf{s})$ for a MIMO IMC design becomes much more complicated than in SISO systems.

- In particular, the key attributes in the synthesis of $\mathbf{Q}(\mathbf{s})$
 - relative-degree (i.e., zeros at infinity)
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Use state space control design!

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- Many control problems require multiple inputs to be manipulated simultaneously in an orchestrated manner. A key difficulty in achieving an appropriate orchestration of the inputs is the multivariable directionality, or coupling.
- Decentralised control might be an option when the plant is diagonally dominant. A practical rule to pair inputs and outputs is based on the **Relative Gain Array**.

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- IMC design for MIMO systems is essentially the same as for SISO systems. Yet, the synthesis process is more subtle, and the required computations may get much more involved.
- We will come back to MIMO systems with State Space System Theory and Control Design.